

BioProcessTM

I N T E R N A T I O N A L

COVERING THE WHOLE DEVELOPMENT PROCESS FOR THE GLOBAL BIOTECHNOLOGY INDUSTRY



■ FOCUS ON

Logistics of Clinical Materials and the Supply Chain

Users Want More from Disposable Connectors

Special Report: BPI Theater at BIO 2014

■ TECHNICAL ARTICLES

Implementing a New Supplement for Fed-Batch Cultures

A New Way to Measure Protein Concentration

Replacing BSA for hMSC Expansion Culture

BPI EXTRA
ONLINE-ONLY CONTENT

■ [Audio Abstracts](#)



Available on the
App Store

Fed-Batch Cell Culture Process Development

Implementing a Novel Nutrient Additive for a Robust, High-Titer, Scalable Process

Meile Liu, Anke Mayer-Bartschmid, Mark Trautwein, Roy Kimura, Karthik Jayapal, Shawn Barrett, Alexander Jockwer, and Paul Wu

The fed-batch culture of Chinese hamster ovary (CHO) cells has become well established as the primary method of manufacturing therapeutic recombinant protein products for various disease indications. Fed-batch process-development approaches focus on supporting high-cell-density cultures that are crucial to achieving high product titers but lead to proportionately high nutritional demands. Exhaustion of key nutrients negatively affects cell growth and ability to produce recombinant proteins. To counter that problem, concentrated feeds are added to the culture. Such feeds tend to be difficult to prepare because of limitations in solubility. Often, high or low pH conditions and/or heating steps must be used to dissolve feed components. In many cases, the resulting solutions have a relatively short shelf life (1, 2).



BAYER HEALTHCARE (WWW.BAYER.COM)

We at Bayer HealthCare implemented a novel, proprietary nutrient additive called GIBCO FunctionMAX TiterEnhancer (Life Technologies, now Thermo Fisher Scientific) in combination with several feeds to enhance CHO cell culture performance. The components were stable and pH-neutral, which contributed to a simple, robust, and good manufacturing practice (GMP)-compliant fed-batch process. Implementing the resulting process has been successfully demonstrated for several different CHO cell lines producing multiple products, all of which have yielded significantly improved titers.

MATERIALS AND METHODS

Cell Lines: We transfected CHO host cell lines — including CHO-S (Life Technologies, now Thermo Fisher Scientific), CHO-K1SV (Lonza Biologics), and CHO-K1 (Sigma-Aldrich) — with monoclonal antibody (MAb) expression vectors. In total, we tested seven different MAb-producing clonal cell lines.

Basal Media and Feeding Solutions: We cultivated CHO-S and CHO-K1SV cells in one of two chemically defined protein free media: CD CHO or CD FortiCHO from Life Technologies (now Thermo Fisher Scientific). We cultured CHO-K1 cells in either ActiCHO (GE HealthCare), HyClone CDM4CHO

PRODUCT FOCUS: ANTIBODIES

PROCESS FOCUS: PRODUCTION

WHO SHOULD READ: QA/QC, PROCESS DEVELOPMENT, MANUFACTURING, AND ANALYTICAL PERSONNEL

KEYWORDS: CULTURE MEDIA AND SUPPLEMENTS, SHAKE-FLASK CULTURE, BIOREACTORS, SCALE-UP, CHO CELLS

LEVEL: INTERMEDIATE

(Thermo Fisher Scientific, now GE Healthcare), or EX-CELL CD CHO Fusion (Sigma-Aldrich) media. Table 1 lists media and feed combinations for each project. In general, we fed CD CHO cultivated cells with CHO CD EfficientFeed A or B supplements (Life Technologies, now Thermo Fisher Scientific) and fed CD FortiCHO-cultivated cells with CD EfficientFeed C (also Life Technologies, now Thermo Fisher Scientific).

In most cases, we added FMTE to those feeds to generate solutions comprising 80% CHO CD EfficientFeed B (EF-B) with 20% FMTE or 70% CD EfficientFeed C (EF-C) with 30% FMTE. For CHO-S and CHO-K1 cells, we supplemented the basal medium with 6 mM glutamine (Life Technologies, now Thermo Fisher Scientific). For project 2, we increased glutamate to 4.5 mM by adding 0.39 g/L glutamate to the CD CHO medium.

And when insufficient glucose was provided by the primary feed solutions, we used a glucose solution of 400 g/L to help maintain targeted glucose concentrations.

Shake Flask and Bioreactor

Operations: Cells were cultured in shaker flasks or stirred-tank bioreactors (Table 1). We seeded the shake-flask cultures at 0.4×10^6 cells/mL for CHO-K1 and 1×10^6 cells/mL for CHO-S cells in 250-mL shake flasks at an initial working volume of 50 mL. A 5% CO₂ humidified incubator maintained cultures at 37 °C, and an orbital shaking platform agitated them at 125 rpm. For CHO-S cells, feeding started on day 3 and repeated every one to three days, with a targeted final glucose concentration at 6–7 g/L. For CHO-K1 cells, feeding started on day 3 and repeated every two to three days, with a targeted final glucose concentration at 7.5–9.0 g/L. We adjusted pH using 6% Na₂CO₃ (EMD

Chemicals) whenever the level fell below 6.9 on the day of sampling.

Cells were also cultivated in bioreactors ranging from 5 L to 1,000 L in capacity (Table 2). The initial working volumes were 65–70% of final volume, with minimal seeding cell densities at $\geq 0.2 \times 10^6$ cells/mL. We used macro-sparging for aeration and dissolved oxygen at 30–40%. Agitation speeds ranged from 30 to 60 rpm, depending on bioreactor volume. To control foaming, we added Antifoam C (Sigma-Aldrich) on demand, prepared as a 100,000-ppm suspension. Depending on the project, initial pH was 6.85–7.10, with temperature at 36.5 °C, and pH and/or temperature were shifted to new set points once cells reached a target density (Table 2). We maintained pH by adding 6% Na₂CO₃ (EMD Chemicals) when needed.

Where we used EF-B + FMTE, feeding was initiated when cells reached $\geq 1.0 \times 10^6$ cells/mL, with a fixed rate of ~2.5% of final volume each day. For projects using EF-C + FMTE, we initiated feeding once cells reached $\geq 4.0 \times 10^6$ cells/mL, with a fixed rate of ~2.9% of final volume each day. Glucose concentration was targeted at 4.5–5.0 g/L, so we used a glucose solution as a supplement whenever necessary. Finally, we terminated and harvested our cell cultures when cell viability reached $\leq 70\%$, generally after 14–17 days of operation.

Analytical Methods: We sampled bioreactors for cell density and viability analysis, using the CEDEX system (Roche Applied Science) to measure nutrient and metabolite concentrations. We determined glucose, lactate, glutamine, and glutamate concentrations using a YSI Model 2700 analyzer (Yellow Springs Instruments). We used a Rapidlab 248 blood gas analyzer (Bayer HealthCare) to measure pH, pCO₂, and pO₂ and a vapor pressure osmometer (Wescor Inc.) to measure osmolality. And we determined IgG concentrations using a titer assay based on high-performance liquid chromatography (HPLC) protein A affinity separation.

Figure 1: Viability cell densities and viabilities of CHO-S cells (Project 1) cultured in CD CHO medium and fed with EF-A, EF-B, or EF-C

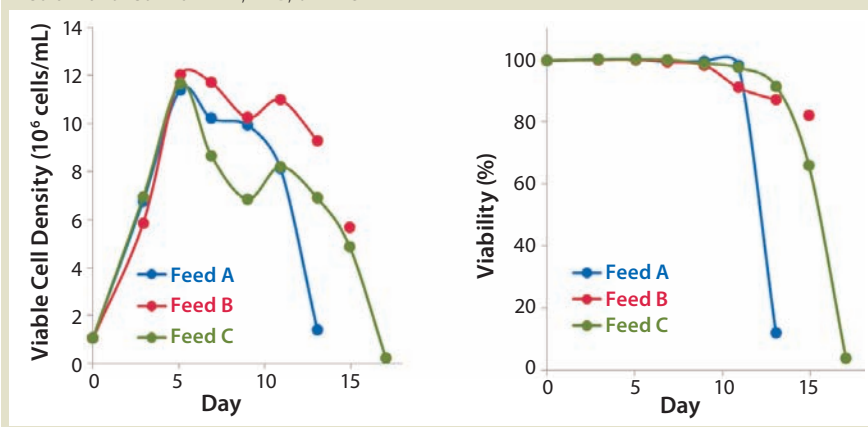
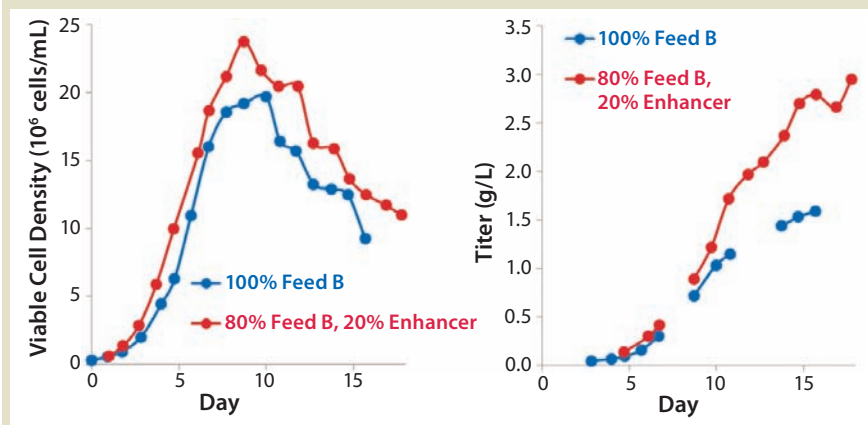


Figure 2: Viable cell densities and titer profiles of Project 2; CHO-K1SV cells were fed with 100% EF-B or a mix of 80% EF-B and 20% FMTE.



RESULTS

Overview of Fed-Batch Operations:

Initially we conducted cell culture process development on CHO-S cells using EF-A, EF-B, and EF-C media. For subsequent projects involving the CHO-K1SV cell line, we added FMTE to EF-B or EF-C to help improve cell culture performance. Finally, we tested those feeds on CHO-K1 cells. Another goal was to establish cell

culture process parameters such as pH and temperature shifts to be coupled with the EfficientFeed media to optimize cell culture output variables, specifically productivity and product quality.

Fed-Batch Process with CHO-S Cell

Line: Table 3 lists the results from each run of CHO-S cells cultured in 250-mL shaker flasks using CD CHO media with 6 mM glutamine and feeding with EF-A, EF-B, or

EF-C. All growth profiles were comparable, with peak viable cell densities (VCDs) of $11\text{--}12 \times 10^6$ cells/mL (Figure 1). Viabilities dropped drastically for cells fed with EF-A and EF-C after 13–14 days of cultivation, whereas viabilities of those fed with EF-B remained >80%.

We harvested the cells on days 13, 15, and 17 for those fed with EF-A, EF-B, or EF-C, respectively. Final osmolality ranged 315–686 mOsm/kg, with the highest measurement belonging to cells fed with EF-C. Lactate remained <2.0 g/L for all cultures, and it was actually produced and then consumed by cells fed according to the EF-A and EF-B regimen. Of the three feeds, EF-C generated the highest MAb titer of 1.8 g/L at harvest, which was close to the satisfactory titer of ≥ 2.0 g/L. It is important to point out that MAb titers for cells fed with EF-B could have been >1.4 g/L if they had been harvested past 15 days because their viability at harvest was still >80%. So we identified EF-B and EF-C as the two potential feeds for our subsequent MAb development projects.

Fed-Batch Culture of CHO-K1SV

Cell Line: Projects 2–6 involved CHO-K1SV cells cultured in bioreactors ranging from 5-L to 1,000-L scales (Table 3). To optimize cell growth and productivity, we developed specific fed-batch process parameters appropriate to the chosen feeding regimens for each individual project. In addition, we introduced the FMTE supplement to these processes, which significantly improved yields and cell performance.

We initially discovered the importance of FMTE in a feed solution in project 2, for which we used a 100% EF-B solution as feed and compared that with the solution of 80% EF-B and 20% FMTE. Without FMTE, the final MAb titer on day 16 was 1.6 g/L, after a peak VCD of 19.7×10^6 cells/mL. In the culture with FMTE included as part of the feed regimen, peak VCD was 23.7×10^6 cells/mL, with a final MAb titer of 3.0 g/L on day 17.

We had to develop specific process parameters for project 2, particularly

Table 1: List of CHO host cell lines, media, and feed combinations, with the fed-batch vessel type and scale evaluated

Project	Cell Line	Media	Feed Type	Vessel Type	Size
1	CHO-S*	CD CHO + 6 mM glutamine	EF-A, EF-B, and EF-C	Shake flask	250 mL
2	CHO-K1SV	CD CHO + 0.39 g/L glutamate	80% EF-B + 20% FMTE	Bioreactor	5 L, 10 L, 200 L, and 1,000 L
3	CHO-K1SV	CD CHO	80% EF-B + 20% FMTE	Bioreactor	10 L and 200 L
4	CHO-K1SV	CD CHO	80% EF-B + 20% FMTE	Bioreactor	10 L and 200 L
5	CHO-K1SV	CD FortiCHO	70% EF-C + 30% FMTE	Bioreactor	5 L, 200 L, and 1,000 L
6	CHO-K1SV	CD CHO	80% EF-B + 20% FMTE	Bioreactor	5 L and 200 L
7	CHO-K1	ActiCHO + 6 mM glutamine	70% EF-C + 30% FMTE	Shake flask	250 mL
		CDM4 + 6 mM glutamine	70% EF-C + 30% FMTE		
		CD CHO Fusion + 6 mM glutamine	40% EF-A + 40% EF-B + 20% FMTE		

Table 2: Fed-batch operational parameters and methods for projects 2–6.

Project	Parameter	Set Points	Feeding VCD	Targeted Glucose
2	DO	30–40%	1.5×10^6	4.5 g/L
	pH	6.9–7.0 (beginning); 6.8 (at start of feeds); 7.0 (lactate consumption and increase in CO ₂ output)		
	Temperature	36.5 °C		
3	DO	40%	1.5×10^6	5.0 g/L
	pH	7.0–7.1 (beginning); 6.8 (at start of feeds); 7.0–7.1 (after temperature shift)		
	Temperature	36.5 °C (beginning); 33.0 °C (starting at $8\text{--}10 \times 10^6$ viable cells/mL)		
4	DO	40%	1.0×10^6	4.5 g/L
	pH	6.85		
	Temperature	36.5 °C		
5	DO	40%	4.0×10^6	4.5 g/L
	pH	7.0		
	Temperature	36.5 °C (beginning); 33.0 °C (starting at $8\text{--}10 \times 10^6$ viable cells/mL)		
6	DO	40	1.5×10^6	4.5 g/L
	pH	7.0 (5 L); 6.95 (200 L)		
	Temperature	36.5 °C		

for implementation of pH shift at appropriate times. Figure 3 shows the two different lactate profiles from project 2. Run 1 was cultivated at pH 6.8 throughout the cell culture period, whereas run 2 was cultivated initially at 6.8 but pH was shifted to 7.0 when feeding started (at $\sim 1.5 \times 10^6$ cells/mL). When cells began to consume lactate and increase their CO_2 output, we shifted the pH back to 7.0 again. That pH shift lowered base addition as well as osmolality, leading to longer and healthier campaigns producing higher MAb titers.

Using the final fed-batch process, we ran project 2 at various bioreactor scales ranging from 5 L to 1,000 L to demonstrate consistencies at different scales (Table 3). Peak VCD was $22\text{--}24 \times 10^6$ cells/mL, and peak lactate was 1.5–1.7 g/L, with all runs demonstrating lactate consumption profiles. Osmolality remained low throughout these campaigns, and final osmolality values were <300 mOsm/kg. Final MAb titers at harvest were >2.0 g/L, with highest titer of 3.0 g/L

achieved at the 5-L scale.

Projects 3–6 also produced desirable growth and productivity profiles under the developed fed-batch processes and feeding regimen (Table 3). For project 3, which used the same 80%/20% regimen as project 2, we implemented pH and temperature shifts at specific time points in the final cell culture process. Final MAb titers for project 3 were between 4.0 and 5.4 g/L, and lactate remained below 2.5 g/L, demonstrated lactate-consumption characteristics (Table 3). Project 6 also used the same feed regimen as project 2, but the specific clone used did not require the pH shift. Nonetheless, MAb titers reached 3.7 g/L at harvest, and those cells also consumed lactate after reaching a peak lactate level <2.0 g/L, in addition to low osmolalities similar to those seen in projects 2 and 3 (Table 3).

For project 5, we used a mix of EF-C and FMTE mix and incorporated a temperature shift into the fed-batch process. Figure 4 shows

growth and titer profiles that resulted under temperature and no temperature shift. As a result of the temperature shift, peak VCD was lower but the cell culture duration was prolonged to 17 days, so titers increased to 4.4 g/L. We also ran project 5 at the 200-L and 1,000-L scales, which also achieved titers >3.0 g/L (Table 3). The 200-L peak VCD was lower than that of the 5-L and 1,000-L scales because the 200-L temperature shift happened at $\sim 8.0 \times 10^6$ cells/mL rather than at 10.0×10^6 cells/mL in the 1,000-L culture. Nevertheless, lactate and osmolality results remained relatively similar across all three scales (Table 3).

Fed-Batch Culture of CHO-K1 Cell

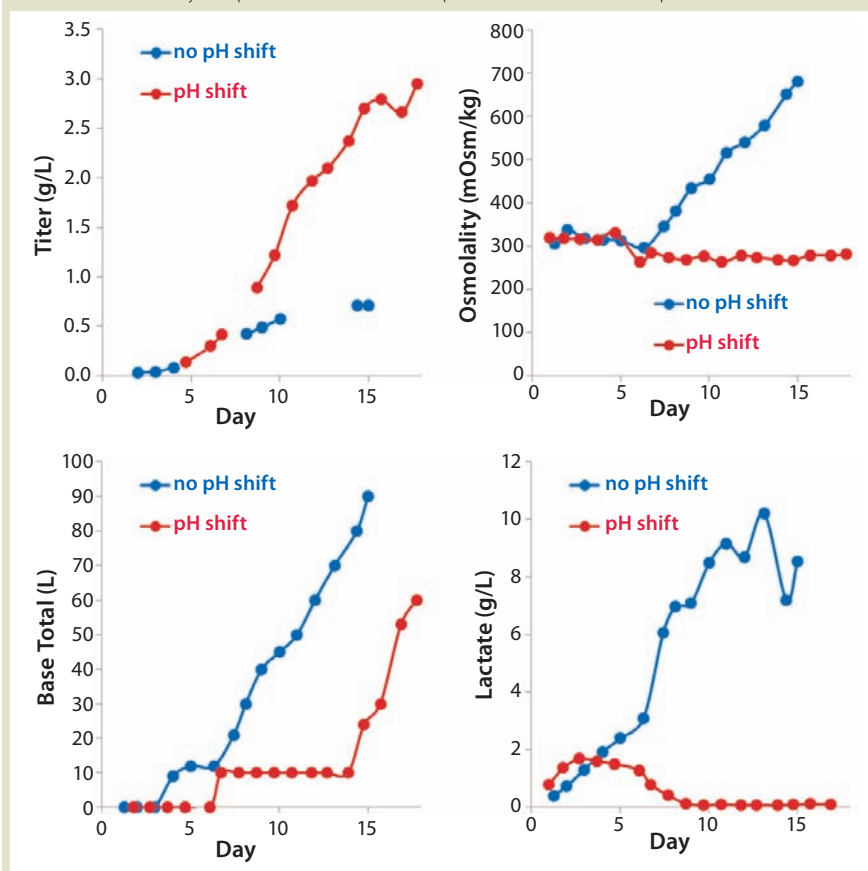
Line: Table 3 lists results from CHO-K1 cells fed with mixes of EF-A, EF-B, EF-C, and FMTE and shows the three best medium and feed combinations discussed herein. The mix of ActiCHO and EF-C/FMTE yielded a final MAb titer of 3.5 g/L by day 14 of cultivation. Peak VCD was 9.6×10^6 cells/mL, and peak lactate reached only 1.4 g/L. The mix of CDM4CHO medium and EF-C/FMTE generated a MAb titer of 5.3 g/L at day 19 of cultivation. The mix of EX-CELL CD CHO Fusion medium and EF-A/EF-B/FMTE yielded final MAb titers of 4.8 g/L by day 21 of cultivation. Similar to the ActiCHO culture, those runs also had peak VCDs around 9×10^6 cell/mL and low lactate profiles throughout.

DISCUSSION

Benefits of Fed-Batch Strategy Using

FMTE: Process development work involving three different CHO cell lines and seven different antibody projects has resulted in an effective fed-batch platform process with many attractive features, including simplicity in preparation and administration of feeds, especially using the novel FMTE nutrient additive. Feeds are added continuously at a fixed flow rate, with no additional bolus feeds required during the culture period. In addition, components dissolve easily during preparation (without the need for heating or cooling), and a neutral pH is maintained throughout that

Figure 3: Titer, osmolality, base addition, and lactate profiles for project 2 show possible differences caused by the presence or absence of pH shift in the fed-batch process.



process. The feeds remain stable for over three months in their liquid form, and we believe that the overall cost of raw materials is lower than for other fed-batch processes currently used in the industry.

Another benefit of our new platform

process is its ability to yield desirable process outputs. For the seven different projects discussed herein, low lactate and low osmolality provided a less stressful culture environment for cultured cells, allowing for sustained high viabilities and extended culture

length — which in turn facilitated higher MAb titers (3–5). Overall, we obtained MAb titers of >2.0 g/L, with 5.3 g/L being the highest measured. These outcomes demonstrate the flexibility of pairing the identified feeds with multiple media types to

Figure 4: Viable cell density, viability, and titer profiles for project 5 show possible differences caused by the presence or absence of temperature shift in the fed-batch process.

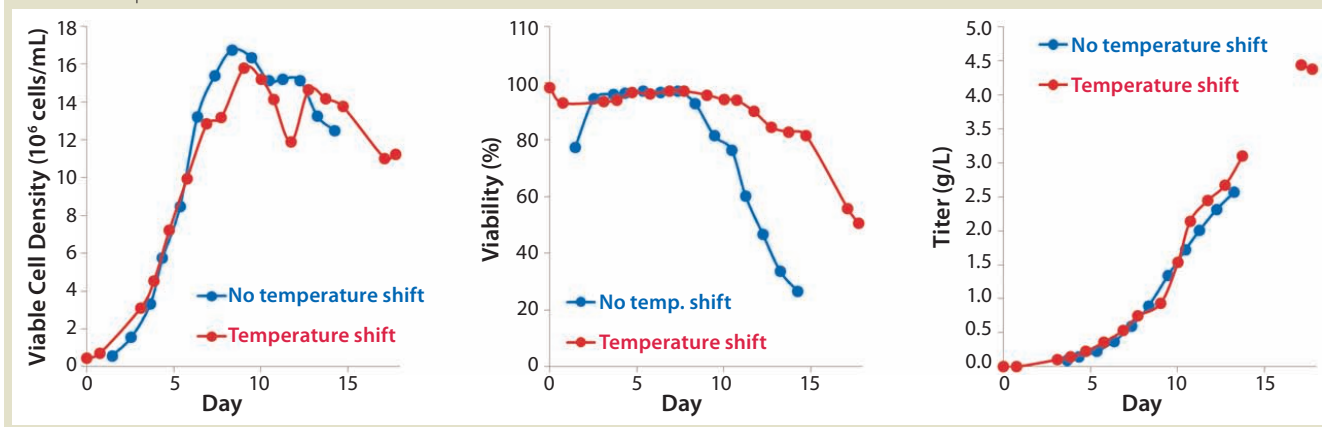


Table 3: Data summary of shaker flask and bioreactor runs of Chinese hamster ovary (CHO) host cell lines for seven different MAb projects evaluated

Project	Cell Line	Process		Temp Shift	pH Shift	Scale	Campaign Length	Peak VCD ^a	Peak Lactate	Final Lactate	Final Osmo ^b	Viability at Harvest	Final IgG Titer		
		Basal Media	Feed												
1	CHO-S*	CD CHO + 6 mM glutamine	EF-A	No	No	250 mL	13 days	11.4	1.3 g/L	1.1 g/L	415	12.2%	0.9 g/L		
			EF-B				14 days	12.0	1.2 g/L	0.2 g/L	315	81.9%	1.4 g/L		
			EF-C				17 days	11.7	1.6 g/L	1.6 g/L	686	4.0%	1.8 g/L		
2	CHO-K1SV	CD CHO + 0.39 g/L glutamate	80% EF-B + 20% FMTE	No	Yes	5 L	16 days	23.7	1.7 g/L	0.1 g/L	281	67.4%	3.0 g/L		
						10 L	17 days	22.0	1.5 g/L	0.1 g/L	276	66.8%	2.8 g/L		
						200 L	14 days	23.8	1.6 g/L	0.1 g/L	260	74.5%	2.1 g/L		
						1,000 L	14 days	21.7	1.5 g/L	0.1 g/L	252	71.2%	2.3 g/L		
3	CHO-K1SV	CD CHO	80% EF-B + 20% FMTE	Yes	Yes	10 L	24 days	12.4	2.4 g/L	0.1 g/L	278	83.9%	5.4 g/L		
						200 L	17 days	11.2	1.8 g/L	0.04 g/L	276	88.2%	4.0 g/L		
4	CHO-K1SV	CD CHO	80% EF-B + 20% FMTE	No	No	10 L	14 days	22.8	1.9 g/L	0.1 g/L	N/A	94.5%	2.6 g/L		
						200 L	14 days	22.7	1.7 g/L	0.1 g/L		94.4%	2.5 g/L		
5	CHO-K1SV	CD FortiCHO	70% EF-C + 30% FMTE	Yes	No	5 L	17 days	15.8	1.4 g/L	0.6 g/L	370	75.3%	4.4 g/L		
						200 L	17 days	13.8	1.3 g/L	0.2 g/L	345	77.0%	3.1 g/L		
						1,000 L	17 days	18.0	1.4 g/L	0.3 g/L	354	88.5%	4.1 g/L		
6	CHO-K1SV	CD CHO	80% EF-B + 20% FMTE	No	No	5 L	17 days	20.6	1.8 g/L	0.1 g/L	257	74.7%	3.7 g/L		
				No	Yes	200 L	16 days	27.3	1.6 g/L	0.1 g/L	N/A	80.4%	3.3 g/L		
7	CHO-K1	ActiCHO+ 6 mM glutamine	70% EF-C + 30% FMTE	No	No	250 mL	14 days	9.6	1.4 g/L	1.4 g/L	N/A	49.7%	3.5 g/L		
		CDM4 + 6 mM glutamine							19 days	8.7	2.57 g/L	2.2 g/L		70.9%	5.3 g/L
		CD CHO Fusion + 6 mM glutamine				40% EF-A + 40% EF-B + 20% FMTE			21 days	8.8	0.9 g/L	0.1 g/L		69.2%	4.8 g/L

^a (10⁶ cells/mL)

^b mOsm/kg

generate satisfactory results.

Process Refinements for Better Performance: Media and feed components are the main elements of our fed-batch process, but we needed to refine that process for it to achieve optimal performance. For example, we established specific process parameters for projects 2–6, including pH and temperature shifts at appropriate times during cultivation. Without a pH shift in project 2, we observed inconsistent cell culture profiles (particularly in lactate and MAb production) between cultures despite the same feed and media being used for all runs. Adding a temperature shift in projects 3 and 5 prolonged cultivation duration to allow for higher MAb titer concentrations at harvest. Although not discussed in detail herein, we increased glutamate in the basal medium for project 2 because it would be completely depleted during the campaign without that additional glutamate supply. Combining these process refinements with the FMTE supplement greatly improved the effectiveness of our media and feed components on the cell culture performance of antibody-producing CHO cells.

Scalable and Robust Performance for Clinical Manufacturing: Adoption of our new platform process provided for a simple and GMP-friendly fed-batch process. The reduced number of raw materials involved simplified raw-material inspection needs and reduced the time and efforts required to bring antibody projects to a clinical-manufacturing level. Project 2 required 13 months from clone selection to GMP drug-substance generation and was the first project to

be evaluated on this new platform process. Using the fully established process, project 5 reached GMP drug substance within a year, starting from clone selection. Both projects showed consistent and robust cell culture performance in pilot-scale bioreactors (1,000 L) compared with the 5-L, 10-L, and 200-L bioreactors. Clinical manufacturing campaigns involving projects 2 and 5 demonstrated that the new platform process is scalable with minimal process deviations. So this is a highly robust and GMP-friendly platform that enables production of multiple-kilogram quantities of MAb drug substance for clinical trials.


A NEW PLATFORM

Our fed-batch platform process was extensively developed involving three different CHO host cell lines and seven different projects, with resulting data demonstrating the effectiveness and benefits of the FunctionMAX TiterEnhancer nutrient additive for fed-batch cultivation of MAb-producing CHO cells. By implementing the new platform process, we easily achieved high productivities in addition to other desirable process attributes. The ease of operation and simplicity of the platform process enables the rapid transfer of antibody projects into clinical manufacturing. It has been proven to be a robust, reproducible, and GMP-friendly fed-batch process.

ACKNOWLEDGMENTS

We thank our colleagues in Global Biologics Development groups at Bayer HealthCare for their contributions.

REFERENCES

- 1 Hackera DL, De Jesus M, Wurm FM. 25 Years of Recombinant Proteins from Reactor-Grown Cells: Where Do We Go from Here? *Biotechnol. Adv.* 27(6) 2009: 1023–1027.
- 2 Barrett SL, et al. Attaining Next-Level Titrers in CHO Fed-Batch Cultures. *BioProcess Int.* 10(10) 2012: 56–62.
- 3 Li J, et al. Feeding Lactate for CHO Cell Culture Processes: Impact on Culture Metabolism and Performance. *Biotechnol. Bioeng.* 109, 2012: 1173–1186.
- 4 Schmelzer AE, Miller WM. Hyperosmotic Stress and Elevated pCO₂ Alter Monoclonal Antibody Charge Distribution and Monosaccharide Content. *Biotechnol. Progr.* 18, 2002: 346–353.
- 5 Zhu MM, et al. Effects of Elevated pCO₂ and Osmolality on Growth of CHO Cells and Production of Antibody-Fusion Protein B1: A Case Study. *Biotechnol. Progr.* 21, 2005: 70–77. 

Meile Liu is a process development scientist, Roy Kimura is a senior staff development scientist, Karthik Jayapal was a staff development scientist (now deputy director of cell culture at Sanofi Pasteur), and corresponding author Paul Wu is director of upstream development in cell culture development (global biological development) at Bayer HealthCare, 800 Dwight Way, Berkeley, CA 94710. Mark Trautwein is a senior research scientist in cell and protein sciences; Anke Mayer-Bartschmid is a senior scientist, and Alexander Jockwer is head of upstream development (Global Biological Development) at Bayer HealthCare, Friedrich-Ebert-Straße 217-475, 42117 Wuppertal, Germany. Shawn Barrett is associate director of bioproduction R&D at Thermo Fisher Scientific, 3175 Staley Road, Grand Island, NY, 14072, USA.

Eprinted and posted with permission to Thermo Fisher Scientific Inc from *BioProcess International* September © 2014 Informa.

ThermoFisher
SCIENTIFIC

The world leader in serving science

BIOPRODUCTION



TOGETHER
POWERFUL
ARE YOUR
BIO
PRODUCTION
PARTNER

Single use | Cell culture | Purification | Analytics

Thermo Scientific™ single-use technologies and Life Technologies™ bioprocessing portfolios are now working together to provide you with innovative solutions and exceptional customer service, from drug discovery through large-scale commercial production.

Under Thermo Fisher Scientific, this unity represents decades of expertise and support, offering you a broad range of products for single-use technologies, cell culture, purification, and analytics, so you can choose what fits your needs. Count on us to be your trusted bioproduction partner.

See our complete offering at
lifetechnologies.com/bioproduction

Caution: For manufacturing, processing, or repacking.
© 2014 Thermo Fisher Scientific Inc. All rights reserved. All trademarks are the property of Thermo Fisher Scientific and its subsidiaries unless otherwise specified.

life
technologies

Thermo
SCIENTIFIC